

1 **Life Cycle Assessment of Wind-based Hydrogen Production in Western Canada**

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6

7 **Abstract**

8 Hydrogen is a key input to industrial processes. In western Canada, there is a
9 significant demand for hydrogen for industrial purposes, both to upgrade bitumen and
10 as a chemical agent. The key driver for this research is the need to assess options for
11 the energy industry to lower its carbon footprint by using hydrogen produced from
12 renewable sources. The environmental impacts associated with hydrogen production
13 through water electrolysis using the electricity generated from a wind power plant are
14 evaluated in this paper. A life cycle assessment was done to determine the greenhouse
15 gas (GHG) emissions per unit mass of produced hydrogen by considering the emissions
16 starting from the extraction of wind energy to the production of hydrogen. An uncertainty
17 analysis was conducted to assess the effects of variations of different input parameters
18 on the GHG footprint of hydrogen produced from wind. The total GHG emissions of a
19 wind-based hydrogen production plant are estimated to be 0.68 ± 0.05 kg CO₂ eq./kg H₂,
20 65% of which are from the construction of the wind power system. The results are
21 compared with those of conventional fossil fuel-based systems. The overall GHG
22 emissions from wind-based hydrogen production are about 94% lower than those

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23 associated with hydrogen production through steam methane reforming (SMR). Natural
24 gas-based hydrogen production emissions are mainly found in the plant operation
25 stage. However, for wind-to-hydrogen systems, the manufacturing and installation of the
26 systems have significant environmental impacts. However, the hydrogen produced from
27 wind energy can significantly reduce the GHG footprint of the energy industry.

28

29 **Keywords:** LCA; hydrogen production; electrolysis; wind energy

30

31 **1. Introduction**

32 Global energy consumption is predicted to increase by 56% from 553 EJ in 2010 to 865
33 EJ in 2040 [1]. Renewable energy is the fastest-growing source of energy in the world.
34 Its share of total energy consumption is expected to increase from 11% in 2010 to 15%
35 in 2040. However, fossil fuels continue to supply most of the world's energy demand. In
36 2040, liquid fuels, natural gas, and coal will supply over 75% of the world's total energy
37 use. Liquid fuel consumption is expected to increase from 87 million barrels per day
38 (bbl/d) in 2010 to 115 million bbl/d in 2040 [1]. Canada has shown strong growth in its
39 liquids production with an average increase of 1.8% per year until recently.

40 Liquids are produced from three major sources: oil sands in Alberta; crude oil in the
41 Western Canada Sedimentary Basin (WCSB), which includes Alberta, Saskatchewan,
42 and parts of British Columbia and Manitoba; and offshore oil fields in eastern Canada.
43 Liquids production from the oil sands has increased steadily in recent decades. It
44 represented over 50% of oil production in 2011, with Alberta, one of the key energy-
45 producing provinces in western Canada, being responsible for more than 75% [1]. This

46 industry has a large greenhouse gas (GHG) emissions footprint and is looking for
47 options to reduce it.

48 In 2012, about 1.9 million bbl/d of crude bitumen were produced from three oil sands
49 regions in Alberta: Athabasca, Cold Lake, and Peace River. About 1.0 million bbl/d of
50 crude bitumen was sent for upgrading in 2012. The upgrading of bitumen to synthetic
51 crude oil (SCO) requires vast amounts of hydrogen. Each barrel of bitumen requires 3-
52 4.5 kg of hydrogen for upgrading [2]. There are currently five operating bitumen
53 upgraders in Alberta, and they have a total capacity of 1.3 million bbl/d [3]. Bitumen
54 upgrading volumes are forecast to rise to 1.5 million bbl/d by 2030 [4]. At present, most
55 of the upgrading operations rely on hydrogen production through steam methane
56 reforming (SMR) [5].

57 Alberta has the highest GHG emissions in Canada. Its total GHG emissions in 2011
58 were 246 Mt CO₂ eq., which represented 35% of the national total [6]. The oil sands
59 operations sector was reported as having the largest share of Alberta's 2011 GHG
60 emissions, emitting 39.8% of total reported emissions [7]. GHG emissions from
61 hydrogen production through SMR are estimated to be 11.89 kg CO₂ eq./kg H₂ [8]. The
62 emissions associated with bitumen upgrading are expected to rise from 18 Mt CO₂ eq.
63 in 2011 to 29 Mt CO₂ eq by 2030 [9]. As GHG emissions associated with hydrogen
64 production are significant, the development of cleaner, more sustainable methods of
65 hydrogen generation are essential for Alberta's oil sands industry.

66 Various methods of hydrogen production from renewable energy resources have been
67 studied [10-19]. Chaubey et al. [12] reviewed the recent developments in industrial
68 techniques for hydrogen production. Among the different methods, water electrolysis is

69 a proven and mature technology in which electricity is used to split water into oxygen
70 and hydrogen. Patyk et al. evaluated the environmental performance of different
71 hydrogen production systems through high temperature electrolysis [20]. A life cycle
72 assessment (LCA) for a high temperature water vapor electrolysis for hydrogen
73 production through a nuclear plant was studied by Utgikar et al. [21]. Thermal-to-electric
74 efficiency of the nuclear plant was assumed to be 45%. The plant's GHG emissions
75 were reported to be 2 kg CO₂ eq./kg H₂.

76 Wind energy is one of the most cost-effective forms of renewable energy with current
77 technology. Alberta has an abundant wind energy resource that can be used to produce
78 the electricity and hydrogen required for bitumen upgrading [22]. As of July 2013, there
79 were 1,088 MW of wind capacity connected to the Alberta grid, which represented about
80 7% of Alberta's total generation capacity of 14,422 MW [22]. There could be
81 approximately 2,200 MW of wind power connected to the grid by 2022 [23].

82 Table 1 presents the wind farms in Alberta that are currently connected to the grid [24].
83 Olateju and Kumar [25] developed a techno-economic model to determine the cost of
84 hydrogen production from wind energy. The Summerview wind farm in Pincher Creek,
85 Alberta was considered in their study. An electrolyzer size of 50 Nm³/h was shown to be
86 the optimal size for a constant flow rate electrolyzer.

87 Large-scale hydrogen production from wind energy was also studied by Olateju et al.
88 [26]. It was shown that the optimal plant configuration would consist of 80 units of 760
89 Nm³/h electrolyzers with a hydrogen production cost of \$8.43/kg H₂.

90 A life cycle assessment of wind-based hydrogen production was conducted by Spath
91 and Mann [27]. Three 50 kW wind turbines with a 30 Nm³/h electrolyzer were
92 considered. The electricity-to-hydrogen efficiency of the electrolyzer was 85%, on a
93 higher heating value basis. Transmission losses of 7.03% were also considered. The
94 produced hydrogen was compressed to a pressure of 20 MPa and stored. The overall
95 GHG emissions were reported as 0.970 kg CO₂ eq./kg H₂ [27]. No publication has been
96 found on an LCA of wind-based hydrogen production specific to western Canada.

97 The overall objective of this paper is to assess the GHG emissions associated with the
98 full life cycle of hydrogen production through water electrolysis using the electricity
99 generated from a wind power plant in western Canada. The specific objectives are to:

- 100 • Conduct an LCA for the production of hydrogen from wind energy in western
101 Canada considering all the unit operations.
- 102 • Compare the LCA results with fossil fuel-based hydrogen production.
- 103 • Conduct an uncertainty analysis to assess the impact of input data on the results.

- 104 • Develop information to better understand hydrogen production using wind energy
105 and make decisions on alternative energy pathways for hydrogen production
106 from wind.

107 **2. Approach and methodology**

108 **2.1 Life cycle assessment**

109 A life cycle assessment (LCA) evaluates the environmental aspects of a product system
110 from raw material acquisition to final disposal. It consists of four phases, as follows [28]:

- 111 - The goal and scope definition, including the reasons for performing the study, the
112 functional unit, and the system boundary.
- 113 - Inventory analysis, including data collection and the quantifying inputs and
114 outputs of each unit operation.
- 115 - Impact assessment, in which the significance of potential environmental impacts
116 is evaluated.
- 117 - Interpretation, that is, the findings from the inventory analysis and the impact
118 assessment phases are considered together to present consistent results based
119 on the goal and scope definition phase of the study.

120 The main life cycle stages and system boundary examined in this study are shown in
121 Fig. 1. The main unit operations studied are wind power generation, hydrogen
122 production through water electrolysis, hydrogen compressions, and hydrogen
123 transportation. Each stage includes manufacturing, transport and erection, operation
124 and maintenance, dismantling, and scrapping. The functional unit is one kilogram (kg) of
125 hydrogen delivered to the bitumen upgrader.

126 **3.2 Uncertainty analysis**

127 A major problem regarding life cycle assessment is the uncertainty of the data used in
128 the inventory analysis. Different techniques are available to estimate uncertainties in the
129 life cycle assessment. A framework for data uncertainty analysis in an LCA was
130 presented by Huijbregts et al. [29]. Data uncertainty is divided into two categories: (1)
131 absence of data, and (2) the inaccuracy of data. Applying uncertainty factors, using
132 input-output modelling, and stochastic modelling are potential options to deal with data
133 inaccuracy for an uncertainty analysis [29]. Stochastic modelling done through a Monte
134 Carlo simulation is a favourable technique to deal with data uncertainty in an LCA [29].
135 Among various available Monte Carlo simulation risk analysis add-ins, ModelRisk is
136 selected and used in this paper [30].

137 **3. Input data and assumptions**

138

139 **3.1 Wind power generation**

140 The Summerview 2 Wind Facility was selected for this study. The facility is located
141 northeast of Pincher Creek, Alberta and is comprised of 22 Vestas V90-3 MW turbines
142 on 80 m towers with a total capacity of 66 MW [31]. The technical specifications of a
143 Vestas V90-3 MW wind turbine are presented in
144 Table 2 [32]. With an average capacity factor of 30% [33], the total electric power
145 generation of the plant is about 173 GWh/y.

146 Table 3 shows the material breakdown for a wind power plant of V90-3.0MW turbines.
147 The electricity grid factor for Alberta, 0.65 t CO₂ eq./MWh, was used for the
148 manufacturing stage [34].

149 **3.2 Water electrolysis**

150 The production of hydrogen through water electrolysis is a critical part of the integrated
151 wind-to-hydrogen system. There are three types of electrolyzers available: alkaline,
152 polymer electrolyte membrane (PEM), and high temperature solid oxide electrolyzers
153 (SOE) [35].

154 Alkaline water electrolysis is a mature technology. Since these electrolyzers are reliable
155 and safe, they are considered the most extended electrolysis technology at the
156 commercial level in the world [35].

157 An alkaline electrolyzer was selected for hydrogen production in this study [25]. The
158 main parameters of this electrolyzer are presented in Table 4. With an electricity-to-
159 hydrogen efficiency of 74% on a higher heating value basis, the rate of hydrogen
160 production is 6.5 t/d. The data presented in [36] are used to evaluate the material and
161 energy consumption for the production of electrolysis.

162 **3.3 Hydrogen compression**

163 The material and energy consumption for the hydrogen compression is presented in
164 Table 5. The energy consumption is calculated based on the exit pressure of the
165 compressor which is considered to be 60 bar [26]. The compressor has an efficiency of
166 70% and lifetime of 22 years [36].

167 **3.4 Hydrogen transportation**

168 Hydrogen is transported from the integrated wind-to-hydrogen plant to the bitumen
169 upgrader through pipeline [36]. The length of the pipeline is estimated as 400 km. The
170 pipeline diameter was calculated by a model developed by Ogden [37]. The lifetime of
171 hydrogen pipeline was assumed to be 22 years [38].

172 **4. Results and discussions**

173 Figure 2 shows the GHG emissions associated with the various stages of wind power
174 generation. The results are presented per unit mass of hydrogen produced by wind-
175 based electricity. GHG emissions of a wind power plant are calculated to be 0.44 kg
176 CO₂ eq./kg H₂. It is observed that the manufacturing stage contributes significantly to
177 the life cycle GHG emissions. The production of the tower, nacelle, and foundations are
178 the principal constituents contributing to GHG emissions. Plant operation contributes
179 about 7% of the total GHG emissions. The end-of-life stage provides an environmental
180 credit of 52% due to avoided metal production of aluminium, iron, copper, and steel.

181 Figure 3 shows the overall emissions associated with the integrated wind-to-hydrogen
182 system and a breakdown of emissions. The plant's total GHG emissions are 0.68 kg
183 CO₂ eq./kg H₂. About 65% of the total integrated plant emissions come from the wind
184 power plant. This is due to the steel and iron materials required for its manufacturing
185 stage. Hydrogen compression, water electrolysis, and hydrogen transportation account
186 for 22%, 7%, and 6% of the total GHG emissions of the plant, respectively.

187 Life cycle emissions from wind-based hydrogen production may be compared with
188 those associated with hydrogen production through steam reforming of natural gas.
189 Overall GHG emissions of the natural gas steam reforming system (SMR) were
190 reported to be 11.89 kg CO₂ eq./kg H₂ [8]. As expected, the GHG emissions associated
191 with fossil fuel-based hydrogen production are mainly in the plant operation stage. The
192 operation stage of a SMR hydrogen production plant contributes to about 75% of the
193 total emissions of the plant. However, GHG emissions of hydrogen production through

194 wind-based electrolysis are 0.68 kg CO₂ eq./kg H₂, which are 94% lower than those of
195 an SMR.

196 **4.1 Uncertainty analysis**

197 An uncertainty analysis was performed by building a Monte Carlo simulation model
198 through ModelRisk. Table 6 shows the variations in key input parameters. The results
199 for the overall GHG emissions are presented in Fig. 4. As can be seen, with a 95% level
200 of confidence, GHG emissions of the plant range between 0.66 and 0.77 kg CO₂ eq./kg
201 H₂.

202 A sensitivity analysis was conducted to better understand the importance and scale of
203 uncertainties in data for a wind-to-hydrogen plant. The lifetime of the plant is 20 years;
204 however, this value may change depending on operating conditions. A sensitivity
205 analysis was conducted to study the impact of variations in plant lifetime on the GHG
206 emissions. The results show that GHG emissions increase by about 26% for a reduced
207 lifetime of 4 years and decrease by 16% for an increased lifetime of 4 years.

208 High wind condition is considered as the baseline case for the LCA. The output
209 electricity is reduced by about 20% if the wind turbine is operated under medium wind
210 conditions. A sensitivity analysis was performed to investigate the changes in
211 construction of the foundation and the tower when moving from high wind conditions to
212 medium wind conditions. The results indicate a substantial increase of 26% in GHG
213 emissions.

214 As stated earlier, the total GHG emissions of the plant range from 0.66 to 0.77 kg CO₂
215 eq./kg H₂. It is important to know which of the unit operations causes this uncertainty.
216 The tornado chart in Fig. 5 shows the degree that the mean of the total emissions is

217 affected by each unit operation distribution. It is observed that the wind power plant's
218 emissions drive the total emissions uncertainty the most. The total GHG emissions
219 range from 0.66 to 0.77 kg CO₂ eq./kg H₂ depending on the emissions from the wind
220 power plant. This range is 0.70-0.72 kg CO₂ eq./kg H₂ for hydrogen compression and
221 0.70-0.71 kg CO₂ eq./kg H₂ for hydrogen production and hydrogen transportation. The
222 total GHG emissions of the integrated wind-to-hydrogen plant are estimated to be
223 0.68±0.05 kg CO₂ eq./kg H₂.

224 **5. Conclusions**

225 The environmental aspects of hydrogen production using wind energy were studied in
226 this paper. A life cycle assessment (LCA) was done to evaluate GHG emissions per unit
227 mass of produced hydrogen considering the various stages of wind-to-hydrogen plants.
228 An uncertainty analysis of the results was also performed. The results show that wind
229 power generation has the most significant effect on the total GHG emissions
230 uncertainty. Therefore, it is worth investigating the possibility of reducing the uncertainty
231 on wind power plant's emissions.

- 232 • The results for life cycle emissions were compared with those of conventional
233 fossil fuel-based systems. The total GHG emissions of a wind-based hydrogen
234 production plant are estimated as 0.68±0.05 kg CO₂ eq./kg H₂, which are about
235 94% lower than those of a natural gas steam reforming system for hydrogen
236 production. The environmental impacts associated with fossil-fuel based
237 hydrogen production are mainly in the plant operation stage. However, for wind-
238 to-hydrogen systems, while there are almost no direct emissions during
239 operation, manufacturing and installation have significant environmental impacts.

240 65% of the total GHG emissions of the integrated wind-to-hydrogen plant come
241 from the wind power generation unit.

242 The results presented in this paper contribute to a better understanding of wind-based
243 hydrogen production processes and provide information that assists in decision-making
244 on alternative energy pathways.

245

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Table 1. Alberta's wind farms¹

Wind Farm	Year Installed	Turbines	Total Installed Capacity (MW)
Ardenville	2010	23XVestas V90-3 MW	69
Blue Trail	2009	22XVestas 3 MW	66
Castle River	2000	15XVestas V47-660 kW	39
	2001	44XVestas V47-660 kW	
Castle Rock	2012	33 X Enercon	75.9
Cowley Ridge	1993	57 X Kenetech 375 kW	40.9
	2001	15 X Nordex 1.3 MW	
Taber	2007	37XEnercon E70 2.2 MW	81.4
Ghost Pine	2010	51X GE 1.6	81.6
Halkirk	2012	83XVestas V90-1.8 MW	149.4
Kettles Hill	2006	5XVestas V80-1.8 MW	63
	2007	30XVestas V80-1.8 MW	
McBride Lake	2003	114XVestas 660 kW	75.2
Soderglen	2006	47XGE 1.5 MW	70.5
Summerview 1	2004	39XVestas 1.8 MW	70.2
Summerview 2	2010	22XVestas 3 MW	66
Chin Chute	2006	20X1.5 MW GE	30
Magrath	2004	20X1.5 MW GE Wind	30
Wintering Hills	2011	General Electric x 55	88

¹ Data presented in [26] are updated based on [24]

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Table 2. Technical specifications of a Vestas V90-3 MW turbine¹

Number of blades	3
Hub height (m)	80
Cut-in wind speed (m/s)	4
Nominal wind speed (m/s)	15
Cut-out wind speed (m/s)	25
Rated output (MW)	3
Nacelle weight (t)	70
Rotor weight (t)	41
Tower weight (t)	160

¹ Derived from [32]

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Table 3. Material consumption of the wind power plant studied[†]

Material (kg/kgH ₂)	Turbine	Foundations	Cables	Transformer
Steel and iron materials	5.82×10^{-2}	1.41×10^{-2}	0	1.68×10^{-4}
Aluminum and aluminum alloys	4.49×10^{-4}	0	1.80×10^{-3}	2.25×10^{-4}
Copper	7.30×10^{-4}	0	8.99×10^{-4}	5.62×10^{-5}
Polymer materials	2.25×10^{-3}	5.62×10^{-5}	1.40×10^{-3}	0
Process polymers	3.37×10^{-4}	0	0	0
Ceramic/glass	2.92×10^{-3}	0	0	0
Concrete	0	2.55×10^{-1}	0	0
Electronics/electrics	5.06×10^{-4}	0	0	0
Lubricants	2.25×10^{-4}	0	0	1.68×10^{-4}

365 [†] Derived from [39] using capacity factor of 30%

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Table 4. Main parameters of the electrolyzer studied[†]

Electricity consumption (kWh/kgH ₂)	53
Water consumption (m ³ /kgH ₂)	0.01
Electricity-to-hydrogen efficiency (%)	74
Temperature (°C)	70
Pressure (bar)	15
Maximum hydrogen production rate (Nm ³ /h)	60
Lifetime (y)	15

368 [†] Derived from [36]

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Table 5. Material and energy consumption for hydrogen compression¹

Material/Energy	Unit	
<i>Compressor</i>		
Chromium steel 18/8	kg/kgH ₂	1.34×10 ⁻³
Cast iron	kg/kgH ₂	4.23×10 ⁻⁴
Ethylene glycol	kg/kgH ₂	4.94×10 ⁻⁶
Lubricating oil	kg/kgH ₂	1.27×10 ⁻⁵
Aluminum	kg/kgH ₂	4.23×10 ⁻⁵
Tube insulation	kg/kgH ₂	1.06×10 ⁻⁵
Copper	kg/kgH ₂	3.17×10 ⁻⁵
Electricity	kWh/kgH ₂	7.05×10 ⁻⁴

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¹ Derived from [36] using the energy consumption calculated in Section 3.3

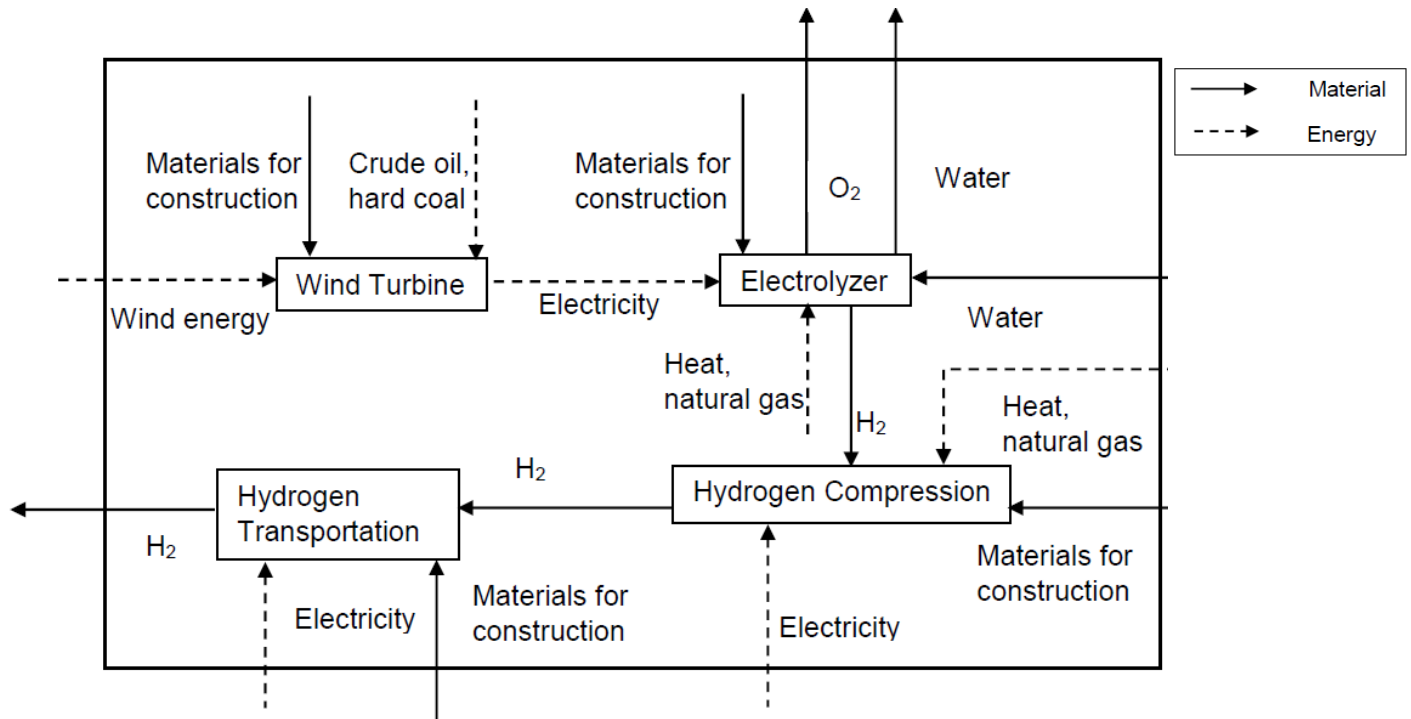
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Table 6. Variation in key input parameters used in uncertainty analysis

Parameter	Unit	Range
Power plant lifetime	y	16-24
Wind speed	m/s	7.5-10
Electrolyzer efficiency	%	70-80
Compressor efficiency	%	70-80
Hydrogen pipeline length	km	100-400

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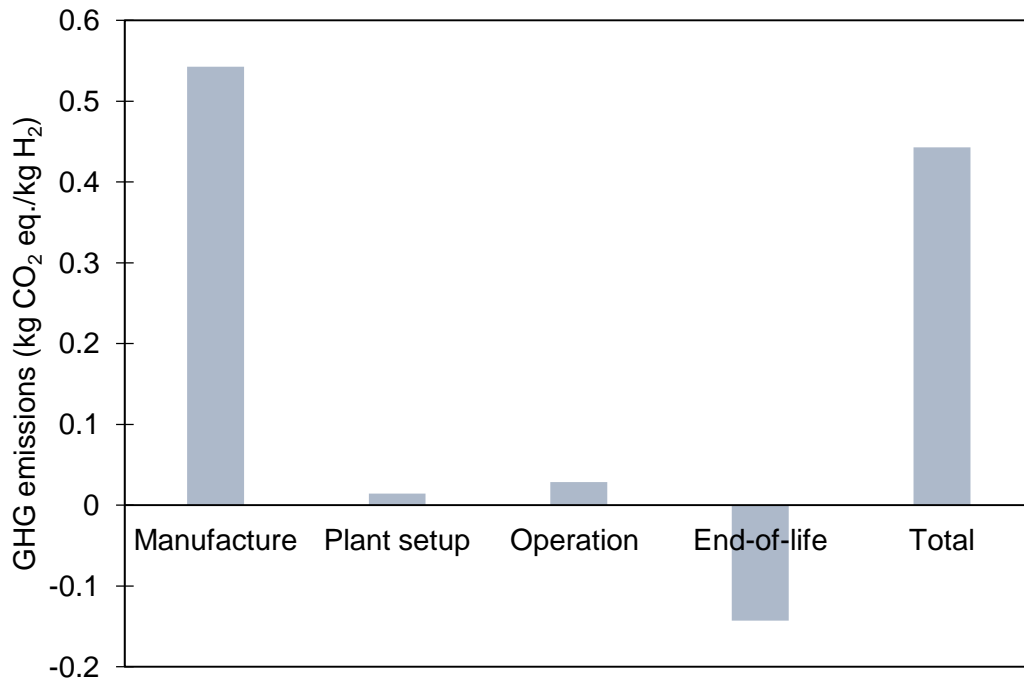
Fig. 1: Life cycle stages for hydrogen production from wind-based electricity

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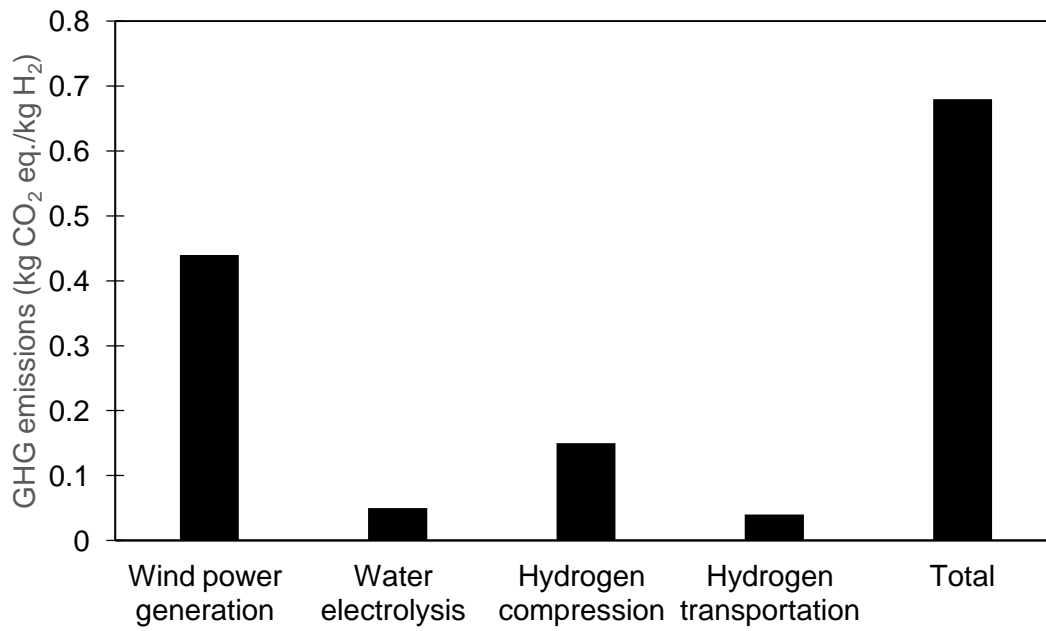
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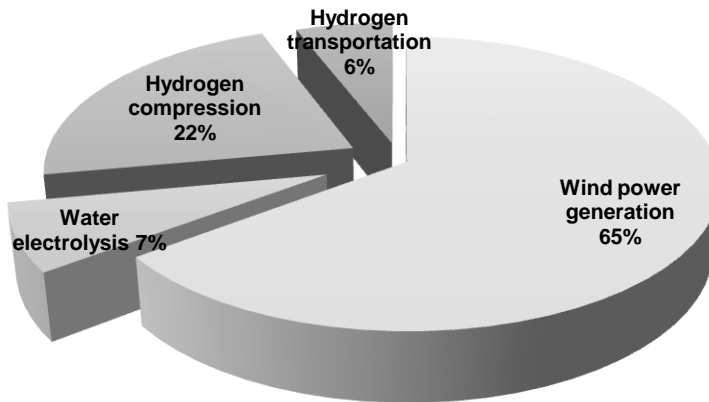
Fig. 2: GHG emissions associated with the various stages of a wind power plant

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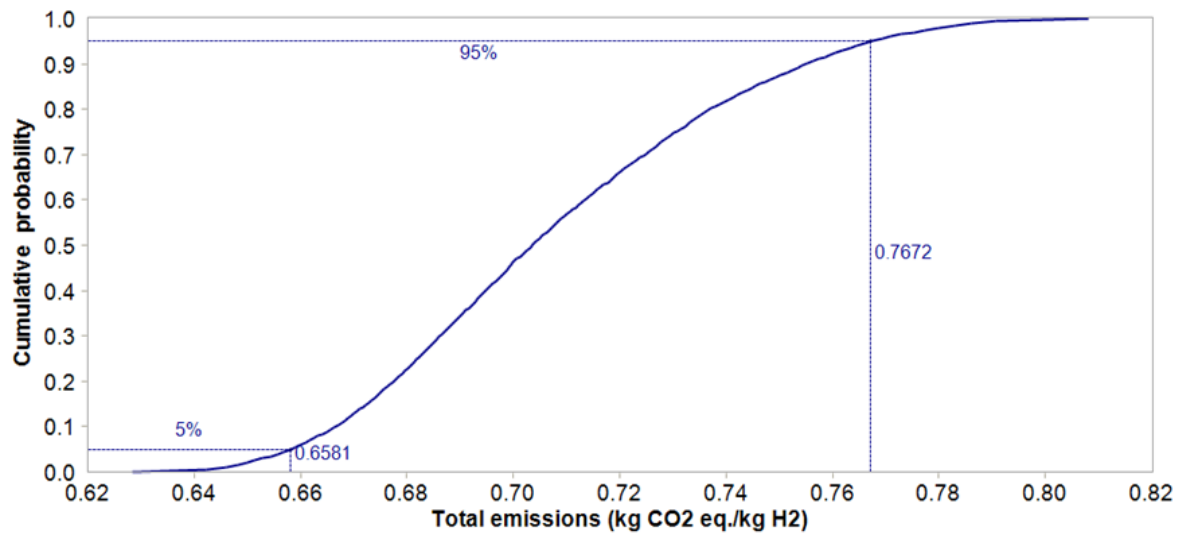


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Fig. 3: GHG emissions of an integrated wind-to-hydrogen system



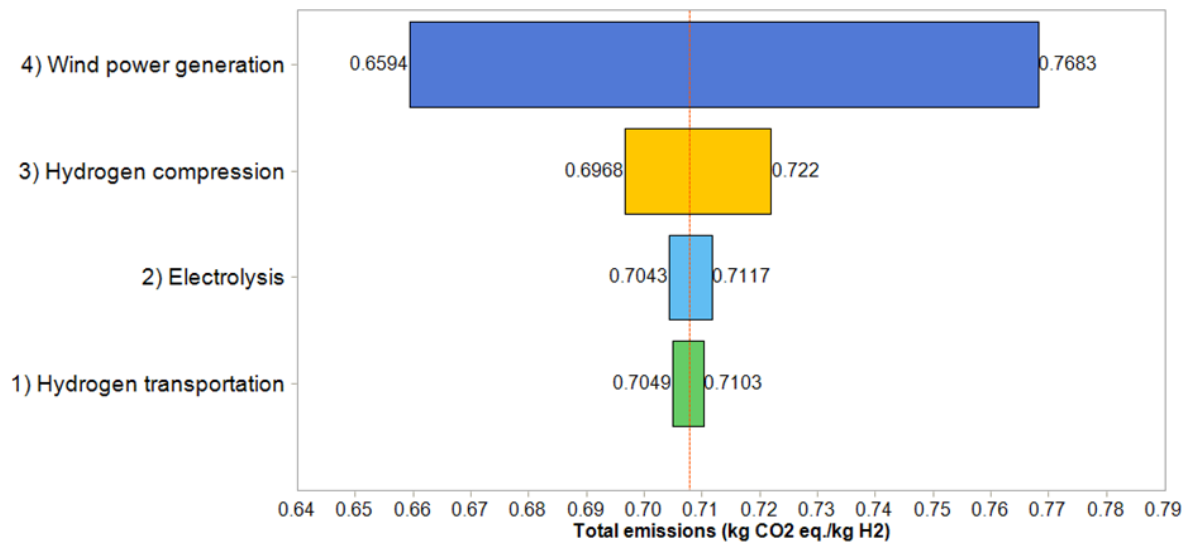
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Fig. 4: Uncertainty analysis with Monte Carlo simulation



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Fig. 5: Tornado plot for total GHG emissions of an integrated plant